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## **CHAPTER 16. SUBCRITICAL WATER EXTRACTION OF BIOACTIVE COMPONENTS FROM ALGAE**

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**Chapter abstract:** Subcritical water extraction (SWE) is presented in this chapter as a potent and novel alternative to conventional solvent extraction processes for isolating bioactive components from algae. SWE is defined as the extraction with water at temperatures ranging from the boiling point to the critical point and at pressures high enough to keep the water in the liquid state throughout the extraction process. Water has many advantages when used as solvent since it is environmentally green and sustainable and can modify some of its physical and chemical properties by heating. Interesting real applications of this technology are discussed together with other applications with potential to be developed successfully under SWE conditions.

**Key words:** subcritical water extraction, pressurized water extraction, algae, SWE, PHWE



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## 17.1 Introduction.

As it has previously mentioned in previous chapters of this book, algae are photosynthetic organisms that can be found in nearly any aquatic and terrestrial habitat. They possess reproductive simple structures and can exist from unicellular microscopic organisms (microalgae) to multicellular organisms of large size (macroalgae). Considering their huge biodiversity and the fact that many species remain unknown, it is easy to understand the interest on the discovery of novel biological active products from algae. Although a lot of research has been carried out on the development of processes for biofuel production using micro- and macroalgae biomass, including those using wastewater as nutrient source (Sturm *et al.*, 2012; Day *et al.*, 2012), another active field of research deals with the use of algae to extract high added value products for the food and pharmaceutical industry (Spolaore *et al.*, 2006). In fact, it has been suggested that secondary metabolites produced by these organisms, when submitted to extreme conditions (changes of salinity, temperature, nutrients, UV-vis irradiation), provide with unique structures with important activities for human health such as antioxidant, antiviral, antimicrobial, hypocholesterolemic, anticarcinogenic, antiallergic, etc. (Li and Kim, 2011; Vo *et al.*, 2012; Javed *et al.*, 2011). Besides, algae can be considered truly natural bioreactors able to grow easily under certain conditions that can be also tuned to produce bioactives at large scale; many applications have been developed dealing with the exploration of marine microorganisms for biotechnological applications, including the production of bioactive compounds for pharmaceutical use, as well as the development of other valuable compounds such as enzymes, nutraceuticals and cosmetics. On the other hand, exploration and use of genomic and metagenomic resources is considered very useful for identification and production of new chemical

structures of commercial interest (Imhoff *et al.*, 2011). Undoubtedly, the combination of these possibilities, together with algae great biodiversity, makes the use of algae an almost unlimited field of research when seeking new bioactive compounds.

Another important aspect to be considered when dealing with obtaining bioactives from algae is the development of appropriate, fast, cost-effective and environmental-friendly extraction processes able to isolate the compounds of interest from these natural sources. In this chapter, we focused on the extraction of bioactives using subcritical water extraction (SWE or PHWE, pressurized hot water extraction). PHWE is a green processing technology using water at high temperature (above its boiling point) and pressure enough to keep water at liquid state at the operating temperature. Water can be considered the *greenest* solvent to work with, it has negligible environmental effect, non-toxicity to health and the environment and it is safe to work with and to transport. Therefore, water is the solvent to select in those applications in which polar protic solvents are needed, although considering the change in water properties with the temperature (for instance, the decrease in dielectric constant with increasing temperature), it is also able to extract medium polarity compounds (Turner and Ibáñez, 2011).

In this book chapter, basic aspects to be considered during SWE (or PHWE) will be discussed, such as the effect of the different factors (temperature, pressure and time) on the process, together with some equipment requirements. Moreover, some real applications of SWE to the extraction of bioactive components, such as antioxidants, from algae will be discussed and compared to traditional processes, while other applications with potential to be developed under SWE conditions will be presented and

critically discussed, with the idea of widening the vision on the possibilities offered by the PHWE technology in obtaining bioactive compounds from algae.

## **17.2 Principles of subcritical water extraction.**

As mentioned, subcritical water extraction (SWE) refers to the advanced extraction technique based on the use of water at high temperatures (higher than the boiling point, 100°C, and lower than the critical temperature, 374 °C) and pressures enough to maintain the waters' liquid state during the whole extraction process. This technique can be considered as a branch of pressurized liquid extraction (PLE), which is based on the same principles but using other solvents to carry out the extractions. As a consequence of the application of these conditions (high pressures and temperatures), faster extraction processes are usually obtained in which the extraction yield is normally higher than the one attainable at room conditions. The use of SWE has been suggested for the extraction of bioactive components from natural sources (Mendiola *et al.*, 2007; Wiboonsirikul and Adachi, 2008; Herrero *et al.*, 2006a). In this section, the influence of the main parameters involved in SWE is briefly described.

### **17.2.1 Extraction Temperature**

Temperature is, undoubtedly, the most influencing parameter in SWE. The increase of water temperature will produce a series of effects, including an improved mass transfer as a result of the increment of the solubility of the compounds present on the matrix being extracted, as well as a decrease on the surface tension of water that allows a better penetration into the sample matrix. The change in viscosity is particularly relevant during the first 100 °C increase of temperature from ambient conditions. Moreover, the

mass transfer kinetics will be also favored by the disruption of intermolecular forces (i.e., van der Waals forces, hydrogen bonds and dipole attractions) in the sample matrix. Nevertheless, the most important effect of the increment of liquid water temperature is the weakening of hydrogen bonds, resulting in a lower dielectric constant ( $\epsilon$ ) (Ong *et al.*, 2006). In fact, this value, taken as a measure of polarity, can vary from 80 (at room temperature) to values around 25 when is submitted to temperatures of ca. 250 °C. This value is similar to the one presented by some organic solvents at room temperature, such as ethanol or methanol (**Figure 1**), and thus, the use of SWE could be an alternative to the use of this type of solvents in some applications.

However, in spite of the above-mentioned advantages, in a real SWE process aimed to the extraction of bioactives from a natural sample, water temperature does not have to be necessarily as high as possible. Instead, this parameter should be optimized and controlled carefully. The main reason is that when using high temperatures, other less desirable effects might also take place. Although, generally, an increase in the temperature produces the subsequent increase in the extraction yield, when dealing with bioactive compounds, too high temperatures could lead to the degradation of these compounds. Thus, the use of experimental designs to optimize the extraction temperature is always recommended. During this process, the qualitative and quantitative presence of bioactive is monitored. For instance, it has been observed how the extraction of phenolic compounds from *Terminalia chebula* plant can be favored with the increasing temperature until 180 °C. Higher temperatures lead to a loss of the phenolic antioxidants (Rangsriwong *et al.*, 2009). Same observations have been reported for other natural antioxidants.

Besides degradations, other reactions might also occur when increasing the extraction temperature. For instance, it has been demonstrated how during SWE processes Maillard, caramelization and/or thermooxidation reactions may occur (Plaza *et al.*, 2010a; Plaza *et al.*, 2010b) considering both, glycation model systems and real natural samples. In fact, it has been shown that the occurrence of those reactions leads to the formation of neoantioxidant compounds not naturally present in the sample being extracted. This point could be an additional advantage, since interesting compounds could be also formed during SWE processes. Nevertheless, caution is recommended in any case, as more studies are needed to assess the safety of the obtained extracts.

### **17.2.2 Extraction pressure**

Pressure has an important effect and function in SWE processes, as it will be the parameter that will permit to maintain the water in the liquid state at high temperatures. For this reason, pressures of 50-100 bar are usually employed. These values are enough to keep the liquid state at the usually employed temperatures. However, although theoretically the pressure might exert a rupture effect on the sample being extracted, several works showed that pressure did not significantly influence the obtained results once it was enough to maintain the water in the liquid state (Herrero *et al.*, 2005).

### **17.2.3 Extraction time**

Extraction time in SWE is referred as the effective time in which the solvent is in contact with the sample being extracted at the desired temperature and pressure conditions. Some commercial instruments apply a heat-up time in order to allow the system to equilibrate at the target conditions. Extraction time starts once the extraction



cell is filled with water at the selected temperature and pressure. In general, the extraction time needed to fully-extract a particular sample will depend on several parameters; one of the most critical is the type of extraction. The most frequent method employed is static extraction in which a certain volume of water, under the desired conditions of pressure and temperature, is maintained in contact with the sample for a given time. Thus, in static conditions, an equilibrium between the sample components still bound to the matrix and the water phase in which the components are already solubilized might be reached. If this is the case, the efficiency of the extraction procedure will not be increased beyond this point. Instead, some compounds' degradations could more easily occur. For this reason the careful optimization of the static extraction time applied is of great importance. In general, relatively short static extraction times (5-20 min) are applied for the extraction of bioactives from natural matrices. On the other hand, if the system is working on a dynamic mode, heated and pressurized water will be flowing into the extraction cell continuously. Theoretically, this mode will be more favorable for the complete extraction of the sample matrix as equilibrium is avoided. However, this dynamic mode is not free of shortcomings; in fact, generally higher volumes of water are employed and sometimes the obtained extract may be too diluted for analytical determination. Besides, if the aim is to achieve a dried extract, the elimination of higher volumes of water (either by freeze-drying or other heat-based methods) will mean more costly procedures.

#### **17.2.4 Other variables**

Besides the above-mentioned most-common variables, other different factors might have an important influence in SWE and, thus, need to be studied during the

optimization of the process. An important variable to be considered if the extraction is performed under dynamic conditions is the flow rate. The flow rate will directly influence the extraction time needed to complete the process. An appropriate flow rate would permit a short contact between sample and solvent allowing the solubilization of the compounds of interest. At the same time it is advisable to have a flow rate not too high so that the extract is not too diluted. Some commercial instruments do not allow performing dynamic extractions. In those cases, the flow rate simply influences the time that will be necessary to have the extraction cell completely filled with pressurized heated water. Another alternative to emulate a dynamic extraction, when working with instruments only permitting static extractions, is the use of sequential extraction of the same sample. By using short extraction times in repeated extraction cycles, higher extraction yields could theoretically be achieved, avoiding the equilibrium between sample components and water. Another possibility is the use of different sequential cycles at diverse extraction conditions. This approach permits the extraction of different kind of components in each temperature step (from lower to higher temperature). It has been already observed that the sequential extraction of natural matrices from low (50 °C) to high (200 °C) temperatures allow the attainment of extracts with different chemical composition (Rodríguez-Meizoso et al., 2006).

Other interesting parameter is the sample physical state. As in every extraction process, the efficiency will be higher as the contact surface is increased. Thus, the sample size should be also studied. Usually, for the extraction of solid dried natural matrices, a grinding procedure is previously performed. The particle size has to be appropriate to maximize the contact surface while avoiding the formation of preferential paths, that is, channels formed inside the extraction cell through which the solvent flows. In some

applications, the introduction of dispersants together with the sample in the extraction cell is employed to favor the uniform distribution of the solvent and to maximize the extraction yield. Of consideration is also the use of in-cell clean-up steps or in-line concentration procedures to improve selectivity. In these cases, the use of adsorbents might be of help in order to retain just some of the extracted compounds while favoring the extraction of the compounds of interest.

### 17.3 Equipment requirements

The basic instrumental requirements to perform SWE are not too complicated. In principle, a pump is needed to pump the water inside the extraction cell as well as to push the extract out, once the extraction is finished. This pump should be capable to achieve the desired pressure (normally, between 35 and 200 bar). The water employed for the extraction should be oxygen-free in order to avoid oxidation of the bioactives as well as to prevent cavitation in the pump. To do that, degassing by ultrasounds or helium purge are commonly employed. The next step will be the extraction cell that should have two on/off valves in order to be able to keep the extraction conditions stable and an oven to heat the extraction cell. The maximum working temperature in most instruments is around 200 °C. Lastly, a collecting vial is needed. Nevertheless, from this starting point, the instrumentation employed might be more or less sophisticated. In **Figure 2** a scheme of a complete SWE device is shown.

For instance, a dynamic extraction might require more accurate pumps in order to maintain a precise flow rate during the whole extraction procedure. Besides, in this case, a heating coil should be included inside the oven so that the water reaches the extraction cell at the set temperature. Although the extraction cell is a simple device, it should be

capable of withstanding high pressures and should include a frit at the exit in order to avoid sample losses. Also, a nitrogen circuit can be included in the system. This circuit can be very useful to purge all the system after the extraction as well as to assure that all the extracting water has reached the collecting vial once the extraction is finished.

There are a number of commercial instruments available in the market, although different applications have been also presented with lab-made instruments. In both cases, it has to be considered that given the operating pressures and temperatures usually employed, corrosive-resistant materials have to be used. For further information on how to build your own system, readers are referred to Turner and Ibáñez (2011)

#### **17.4. Applications to the extraction of bioactive components from algae; comparison with conventional processes.**

As mentioned in the introduction, environmental parameters, such as water temperature, salinity, light and nutrients available can modify the chemical composition of algae and microalgae. For that reason, not only the presence of a particular compound makes algae interesting as source of bioactive compounds but also their huge diversity, the possibility of harvesting or growing at conditions that lead to an enrichment of some bioactives, and the chance of using sophisticated genetic engineering tools able to also produce certain type of compounds (Plaza *et al.*, 2008; Plaza *et al.*, 2009; Johanningmeier and Fischer, 2010; Wijffels, 2008). In the last years several processes have been developed and optimized focused on the extraction of bioactive compounds from algae and microalgae. The composition of those extracts is highly dependent on algae specie, culture and growing conditions and extraction conditions.

### 17.4.1 Antioxidants

Interest in natural antioxidants for both health and improved food stabilization has intensified dramatically since the last decade of the XX century. Health applications have been stimulated by observations that free radicals and oxidation are involved in many physiological functions and cause pathological conditions. In fact, the antioxidant capacity has been related to different disease processes and their prevention such as cancer, coronary heart diseases, inflammatory disorders, neurological degeneration, aging, etc. (Madhavi *et al.*, 1996). On the other hand, natural antioxidants offer food, pharmaceutical, nutraceutical, and cosmetic manufacturers a “green” label, minimal regulatory interference with use, and the possibility of multiple actions that improve and extend food and pharmaceutical stabilization (Schaich, 2006).

Several compounds from marine sources have proven their antioxidant activity both, *in vitro* and *in vivo*. Among them, phenolic compounds can be appropriately extracted using SWE. Phenols are an important group of natural products with antioxidant and other biological activities. These compounds play an important role in algal cell defense against abiotic and biotic stress. Several authors have recently published results regarding the total phenol content and antioxidant activity of algae (Ganesan *et al.*, 2008). The main bioactivity associated to phenolic compounds is antioxidant activity, which is also the main bioactivity of algal and microalgal phenolics (Kumar *et al.*, 2008).

The content and profile of phenolic substances in marine algae vary with the species. While bromophenols are the main antioxidants in red marine algae (Takamatsu *et al.*, 2003), in marine brown algae, a group of polymers called phlorotannins comprises the major phenolic compounds (Chkikvishvili and Ramazanov, 2000) such as fucols,

phlorethols, fucophlorethols, fuhalols and halogenated and sulphited phlorotannins.

Some of the first polyphenols found in algae (*Fucus* and *Ascophyllum spp.*) were phlorotannins. They are formed from the oligomeric structures of phloroglucinol (1,3,5-trihydroxybenzene) (Parys *et al.*, 2007). Also, some flavanone glycosides have been found even in fresh water algae (Konishi *et al.*, 2003).

Although some references can be found in the literature dealing with polyphenol's extraction using water as a solvent (Wang *et al.*, 2009; López *et al.*, 2011), it seems clear that water by itself at low temperatures is not able to provide with similar results as using for instance, ethanol or acetone as extracting solvents. One possibility of increasing polyphenol's extraction efficiency is the use of enzyme-assistant extraction that consists on an enzymatic step previous or simultaneous to water extraction. In this case, the release of polyphenols from algae cell wall structures by using carbohydrate degrading enzymes and proteases has been suggested, for instance, for extracting polyphenols with antioxidant activity from seven species of brown seaweeds (Heo *et al.*, 2005) or red algae (Wang *et al.*, 2010). A review on the use of enzyme-assistant extraction (EAE) on the recovery of industrially important metabolites from seaweeds has recently been published (Wijesinghe and Jeon, 2012a). Another possibility of increasing polyphenol's extraction from algae is the combined use of enzymatic degradation together with extraction with water at high temperatures. By using this combination it would be possible to improve the release of bioactive compounds and to increase the extraction efficiency by both mechanisms, polyphenols release from cell walls or from protein-algal polyphenol complex, and increase of compound's solubility by increasing water temperature and pressure. Although this combination has not been

tested yet in algae, its success in the extraction of valuable compounds from other natural sources such as onion waste, suggest a new use of this approach (Turner *et al.*, 2006).

Other compounds found in algae with important antioxidant properties are carotenoids.

*Haematococcus pluvialis* is a green microalgae well known by its content in antioxidants belonging to carotenoid class (mainly astaxanthin). *H. pluvialis* has been evaluated as a source of other kind of antioxidant compounds using subcritical water as extraction agent (Rodríguez-Meizoso *et al.*, 2010). In a previous work by the same authors (Jaime *et al.*, 2010) other solvents were used also in subcritical conditions, such as hexane and ethanol. The effect of the extraction temperature (50, 100, 150, and 200 °C) and the polarity of the solvent has been estimated in terms of *in vitro* antioxidant activity. Results in both works demonstrated that the extraction temperature had a positive influence in the extraction yield, although its effect in the antioxidant activity was negative, lowering the activity of the extracts with an increase of the extraction temperature when ethanol and hexane were used as extracting solvents. When using water as solvent, the extraction temperature had a positive influence on the antioxidant activity; in this sense, a possible correlation was found between the antioxidant activity and vitamin E, simple phenols (gallate derivatives), caramelization products, and possible Maillard reaction products obtained during the extraction at high temperatures. Nevertheless, the compounds responsible for this activity in the ethanol and hexane extracts were carotenoids (astaxanthin, lutein, etc.).

Certain cyanobacteria such as *Phormidium* have also been tested to obtain antioxidant fractions using SWE (Rodríguez-Meizoso *et al.*, 2008). The subcritical extracts were obtained using water, ethanol and hexane. Four different extraction temperatures were tested (50, 100, 150, and 200 °C) with 20 min as extraction time. TEAC assay was used

to test antioxidant activity of the extracts. In general, hexane and ethanol extracts showed a higher antioxidant capacity that was mainly attributed to carotenoid compounds. On the other hand, the high antioxidant activity of the 200 °C water extracts was likely related to the presence of Maillard reaction compounds.

As can be seen, the antioxidant activity of subcritical water extracts from algae obtained at high temperatures can be partially attributed to the formation of Maillard reaction products during the extraction process. The neoformation of antioxidants during SWE has been verified in microalgae (*Chlorella vulgaris*) and algae (*Sargassum vulgare*, *Sargassum muticum*, *Porphyra spp.*, *Cystoseira abies-marina*, *Undaria pinnatifida* and *Halopitys incurvus*) (Plaza *et al.*, 2010a). Results obtained from this study suggested that neoformed compounds derived from Maillard, caramelization and thermoxidation reactions affect the overall antioxidant capacity of water subcritical extracts depending on the nature of the sample. The brown algae *U. pinnatifida* was the sample in which these chemical events contributed positively to a higher extent.

Among other interesting antioxidant compounds extracted using SWE are phycobiliproteins, which are a group of colored proteins commonly present in cyanobacteria and red algae possessing a wide spectrum of applications. The major organisms exploited for production are the cyanobacterium *Spirulina* for phycocyanin and the red alga *Phorphyridium* for phycoerythrin (Sekar and Chandramohan, 2008). Beside their antioxidant activity, phycobiliproteins have many other uses such as: pigments, fluorescent dyes, anti-inflammatory, neuroprotective and hepatoprotective activity. Several classical extraction methods have been used, including extraction with distilled water, extraction by homogenization in a mortar and pestle in the presence of acid-washed neutral sand using 50 mM sodium phosphate buffer at pH 6.8, extraction



by homogenization in a Virtimixer in 50 mM phosphate buffer at pH 6.8, and extraction with various concentrations of hydrochloric acid (2 to 10 N) at room temperature (Sarada *et al.*, 1999). But in 2004 a fast green method was developed using SWE (Herrero *et al.*, 2004). In this work, the use of water for phycobiliprotein's extraction was compared with other solvents (hexane, light petroleum and ethanol) and extracts were characterized by using micellar electrokinetic chromatography with diode array detection (MEKC–DAD). The presence of phycobiliproteins in pressurized water extracts was confirmed by using CE-MS (Herrero, *et al.*, 2005; Simó *et al.*, 2005). The optimal conditions to extract phycocyanin from *Spirulina* were 1500 psi and 25 °C, using glass beads as packing material and 15 min of extraction time.

#### **17.4.2 Antimicrobials and antivirals**

Besides compounds with antioxidant properties, algae are also a natural source of other compounds with interesting biological activity such as antimicrobials and antivirals, which inhibits the growth or multiplication of microorganisms (Mayer *et al.*, 2009). A large number of algae extract have shown to have antimicrobial activity against microbial species, yeast or fungus (Gupta and Abu-Ghannam, 2011; Caki *et al.*, 2011; Pierre *et al.*, 2011; Khairy and El-Kassas, 2010; Santoyo *et al.*, 2009; Thillairajasekar *et al.*, 2009). However, the antimicrobial activity depends on both algal species and the efficiency of the extraction method. For instance, the diethyl ether extract of *D. linearis* was ineffective against microorganisms, whereas its ethanolic extract showed antimicrobial activity against *gram*-negative bacteria and *Candida sp.* This fact is related to the presence of bioactive metabolites which are soluble in ethanol but not in diethyl ether (Tüney *et al.*, 2006). In spite that the most employed methods for

extracting compounds with antimicrobial activity from alga are still conventional extraction methods employing organic solvents (ethyl acetate, diethyl ether, chloroform, hexane, methanol, ethanol) or water as extraction solvent, several works have been published in the literature dealing with pressurized liquid extraction of antimicrobial compounds from different algae (Herrero *et al.*, 2006b; Rodríguez-Meizoso *et al.*, 2008; Plaza *et al.*, 2010c; Plaza *et al.*, 2012). In all these works, different solvents (including water), covering a wide range of dielectric constants were tested, allowing the evaluation of the influence of the solvent polarity on the extraction of antimicrobial compounds. The extraction yields obtained using subcritical water extraction followed a different behaviour in each algae studied; the lowest extraction yields (comparing with the other solvents tested) were achieved for *Dunaliella salina* and *Phormidium* species (Herrero *et al.* 2006b; Rodríguez-Meizoso *et al.* 2008) whereas the highest values were obtained for *Himanthalia elongata*, *Synechocystis sp.*, and *Chlorella vulgaris* (Plaza *et al.* 2010c; Plaza *et al.* 2012). Regarding the antimicrobial activity of the different extracts obtained in these works, those obtained using water as extraction solvent were the less active against the different microorganisms tested.

Lately, Rodríguez-Meizoso *et al.* (2010) carried out the study of bioactive compounds from *Haematococcus pluvialis* extracted by SWE (Rodríguez-Meizoso *et al.*, 2010). Using a pretreatment based on three freezing-smashing-thawing cycles (to enhance extraction yields), four different temperatures (50, 100, 150, and 200 °C) with 20 min as extraction time were tested. All the extracts obtained showed a good antimicrobial activity against bacteria and yeast and small antifungal activity against *Aspergillus niger*. The analysis of the antimicrobial activity as a function of extraction temperature indicated that the temperature did not really affect the extraction of antimicrobial

compounds from the algae. In addition, the characterization of these extract by GC-MS demonstrated that short chain fatty acids could be responsible of the observed antimicrobial activity.

The fact that algae may produce antiviral compounds is also well-known since different studies have reported a number of compounds from algae extracts with potent antiviral activity (Iwashima *et al.*, 2005; Rodríguez *et al.*, 2005; De Souza *et al.*, 2005; Lee *et al.*, 2006; Soares *et al.*, 2007; Hayashia *et al.*, 2008; Vo *et al.*, 2011). Water or methanol have been usually employed to screen for antiviral compounds from different algae. However, the antiviral potential of most algae remains unknown since this sort of analysis has been carried out only with few species.

Only a few applications can be found in the literature dealing with the ability of pressurized liquid extraction to obtain antiviral compounds from algae such as *Chlorella vulgaris* (Santoyo *et al.*, 2010), *Himanthalia elongata* (Santoyo *et al.*, 2011), *Haematococcus pluvialis* and *Dunaliella salina* (Santoyo *et al.*, 2012). Extractions were performed using different solvents (water, ethanol, and hexane or acetone) under subcritical conditions. Namely, when using *Haematococcus pluvialis* and *Himanthalia elongata*, extractions were performed at 100 °C for 20 min, whereas for *Chlorella vulgaris* and *Dunaliella salina*, extractions were carried out at 150 °C for 20 min and 160 °C for 15 min, respectively. The antiviral properties of the obtained extracts were evaluated against Herpes simplex virus type 1 (HSV-1). The extracts obtained for all the algae studied were able to inhibit HSV-1 intracellular replication as well as disrupt the step of attachment. Regarding water extracts, a higher antiviral activity was shown by the polysaccharides-rich fraction isolated from these extracts compared to the original

water extract. Therefore, polysaccharides present in water extracts could be suggested as the compounds responsible for the antiviral activity.

### **17.4.3 Other bioactive products from algae in the frontier to be extracted**

As mentioned, pressurized liquid extraction, more specifically SWE (or PHWE), is a quite novel extraction process with many interesting applications nowadays. Although this technique has demonstrated its usefulness to obtain bioactive compounds with antioxidant, antimicrobial and antiviral activity from different algae, its possible use as an alternative to conventional extraction methods for some applications has not been demonstrated yet.

In the following sections of the chapter we will study the possibility of using SWE as an alternative to traditional methods for selected applications for which no references have been found. With no doubt, this has to be taken as a possibility since the final usefulness of the technique will need further and serious studies to determine the validity of the process and/or the hypotheses developed and presented in this part. Compounds selected “in the frontier to be extracted” are those that fulfill the requirements for water extraction in terms of high to medium polarity, low basicity and high proticity (Turner and Ibáñez, 2011), that are found in different types of algae and provide with important biological activities; in this sense, carbohydrates, bioactive peptides, neuroprotective compounds, pigments and toxins are discussed.

#### **17.4.3.1 Carbohydrates or Saccharides**

Carbohydrates or saccharides (from the Greek word σάκχαρον (sákkharon), meaning “sugar”) are organic compounds with the empirical formula  $C_m(H_2O)_n$  (where m could

be different from n) highly abundant among marine algae and microalgae. The use of subcritical water to perform integrated processes (extraction, fractionation, reaction...) involving marine carbohydrates could be a future trend to consider. For instance, saccharides have been extracted with subcritical water from non-sea vegetable such as citrus (Tanaka *et al.*, 2012). In fact is in the fractionation step when subcritical water (hydrothermal treatment) could be easily applied to algae and microalgae due to their high content in polysaccharides. Although some information can be found on the hydrothermal processing of agricultural residues, the exact composition of the product streams will be mainly dependent on the starting material (Liu and Wyman, 2003; Pronyk *et al.*, 2011), therefore, there are no possibilities for extrapolating the published results.

On the other hand, polysaccharides from algae have been extensively reviewed and characterized; for instance, during the last three decades, the group of Anatolii Usov, from the Russian Academy of Sciences, published a series of works entitled “Polysaccharides from algae” (Usov *et al.*, 1992; Usov *et al.*, 2001). Among marine polysaccharides, fucoidans and sulfated polysaccharides from brown algae have attracted steady attention in the last few years as readily accessible biopolymers possessing a wide spectrum of biological activities. Fucoidans represent a rather heterogeneous group of polysaccharides in which their simplest representatives contain only  $\alpha$ -L-fucose, sulfate, and acetate (Usov *et al.*, 2001). It is noteworthy that fucoidans isolated from species belonging to different orders of brown algae can differ in the structure of the main chain: in addition to fucose, they contain xylose, galactose, mannose, and glucuronic acid while other polysaccharides, composed for example, of residues of galactose or glucuronic acid and mannose, in which fucose is only a

component of side chains, are also often classified as fucoidans (Jiao *et al.*, 2011).

**Figure 3** illustrates the fucoidans structure from *Fucus vesiculosus*.

Generally polysaccharides from seaweeds have been extracted using water or aqueous organic solvents (Albuquerque *et al.*, 2004), although extraction efficiency will be influenced by the chemical nature of the components, the extraction method employed and the presence of interfering substances (Wijesinghe and Jeon, 2012b). On the other hand, saccharides can be sequentially extracted based on their different solubility. For example, the extraction procedure in the brown seaweed *Fucus vesiculosus* includes water, acid, and alkali treatments (Rupérez *et al.*, 2002); laminarans (linear polysaccharides, with a  $\beta(1\rightarrow3):\beta(1\rightarrow6)$  ratio of 3:1) are extracted using water, although their solubility depend on the branching level, being higher the solubility at higher branching degree. Fucans are extracted with diluted hydrochloric acid, while alginates are extracted with alkali. Alginates form insoluble precipitates of alginic acid at low pH, but they are stable in solution between pH 6 and 9.

On the other hand, sulfated galactans from red seaweeds are soluble in aqueous solution at 20 °C, while those less modified such as agar in Nori (*Porphyra spp.*) are soluble at 60–80 °C (Rupérez and Toledano, 2003). As could be seen, pressurized water could be used to extract algal saccharides, both alone and in combination with acids or alkalis. However, as mentioned previously for polyphenols' extraction, since the cell wall consists of complex polymers, it is not easy to extract active polysaccharides using a conventional solvent extraction process. The production of different bioactive polysaccharides using an enzyme-assisted extraction with lyases increases the extraction efficiency of the process (Wijesinghe and Jeon, 2012b). In this sense SWE could be an interesting alternative to isolate algal polysaccharides since it could be used alone or in

combination with an enzymatic treatment inside the extraction vessel. In addition, the dissociation constant of subcritical water for hydrogen and hydroxyl ions is three orders of magnitude higher than that of ambient water; consequently, subcritical water can act as an acid or an alkali (Wiboonsirikul and Adachi, 2008). This potential has been exploited to extract and hydrolyze polysaccharides from other sources (Sasaki *et al.*, 2000).

#### **17.4.3.2 Bioactive peptides**

Many studies have reported that peptides from various food sources possess bioactivities, including antihypertensive, antioxidant, anticancer, antimicrobial, and opioid activities as well as immunomodulatory and cholesterol-lowering effects (Shahidi and Zhong, 2008). The primary structure of natural proteins consists of certain amino acid sequences that have the ability to exert physiological benefits in human beings. When the parent protein is acted upon by an appropriate enzyme (usually a protease), the peptide is released. When consumed as pure peptides or more likely as a hydrolysate, the active peptides must survive digestion as they pass through the gastrointestinal tract and must be absorbed intact into the blood circulatory system. The peptides are then transported to various organs and tissues where they modulate the structure and function of metabolic enzymes that participate in the pathogenesis of chronic diseases.

Recently, great interest has been expressed regarding marine-derived bioactive peptides because of their numerous health benefits. In addition, many studies have been reported that marine bioactive peptides can be used as functional foods, nutraceuticals, or pharmaceuticals due to their therapeutic potential in the treatment or prevention of

various diseases (Kim and Kang, 2011). *Arthrospira* (*Spirulina*), *Chlorella*, and *D. salina* were used in human nutrition diets because of their high protein content and their excellent nutritive value, therefore this high protein content can be used as a source of bioactive peptides.

Anticancer peptides have attracted attention recently due to their characteristic features such as multifunction, high sensitivity, and stability. Just few studies have been reported about microalgae protein as a source of anticancer peptides (Kim and Kang, 2011), but there are a quite large number of publications on anticancer peptides from food protein from several sources (Udenigwe and Aluko, 2012). However, recent studies suggest that the microalgae-derived peptides could be potentially useful adjuncts in the treatment of gastric cancer (Sheih *et al.*, 2010). Therefore, this can be a potential protein source for the future industrial production of functional peptides.

The angiotensin I-converting enzyme (ACE) participates in regulating blood pressure in the renin–angiotensin system. The ACE-inhibitory activity of various source have studied, and it was found that some ACE-inhibitory peptides were produced by enzymatic digestion of various marine food proteins (Kim and Kang, 2011). However, to date, scarce work of the potential ACE-inhibitory compounds such as biopeptides from seaweeds has been done. The main studied algae for this purpose has been wakame (*Undaria pinnatifida*) (Sato *et al.*, 2002; Suetsuna and Nakano, 2000), whose bioactive peptides from protease digestion have been isolated using solvents such as butanol and column elution with acidified water. Since bioactive peptides are water soluble, they could also be extracted using one step of an integrated procedure combining enzyme-assisted extraction (EAE) and SWE.



### 17.4.3.3 Neuroprotective compounds

Alzheimer's disease (AD) is an irreversible, progressive neurodegenerative disease, which results in memory loss, behavior disturbances, personality changes and a decline in cognitive abilities. It was stated in the cholinergic hypothesis, that a serious loss of cholinergic function in the central nervous system (CNS) contributes significantly to the cognitive symptoms associated with AD. The inhibition of acetylcholinesterase (AChE) enzyme, which catalyzes the breakdown of the neurotransmitter acetylcholine (ACh), may be one of the most realistic approaches to the symptomatic treatment of AD (Tabet, 2006). Otherwise, the use of synthetic AChE inhibitors is under study due to their secondary effects associated with the requirement to be used for long term or indefinitely (depleting neurotransmitter substrate, altering tone of surviving neurons, or just having no effect) (Schneider, 2012). This fact reveals the need of finding new sources of compounds that interact with the cholinergic function.

A number of studies have recently shown AChE inhibitory activity of several marine algae species, such as *Ecklonia stolonifera*, *Ishige okamurae*, *Caulerpa racemosa*, *Ulva*, *Amphiora* or *Hypnea valentiae* (Pangestuti and Kim, 2011a). The main neuroprotective compounds found in algae belong to two families of compounds: sterols and phlorotannins. Most of those bioactivities have been proven using room temperature methanol or ethanol extraction (Stirk *et al.*, 2007; Suganthi *et al.*, 2010; Cho *et al.*, 2012). Therefore in both cases, extractions could be performed using subcritical water, because their extraction could be mediated by the change in polarity (dielectric constant) of water with temperature close to critical point. In addition, a substantial increase in the ionic product during subcritical water extraction, in particular, at temperatures between 120 and 250 °C, contributes to the hydrolysis which enhances the

mass transfer, like the decreasing in the viscosity and surface tension close to the critical point (Wiboonsirikul and Adachi, 2008).

#### **17.4.3.4 Pigments**

Among functional ingredients from algae, pigments have received particular attention. Besides their photosynthetic and pigmentation effects, these pigments exhibit different health benefit, such as antioxidant, anticancer, anti-inflammatory (Pangestuti and Kim, 2011b). Carotenoids, chlorophylls and phycobiliproteins are the basic classes of pigments that can be found in algae. According to the pigment content, algae can be classified into brown (*Phaeophyceae*), red (*Rhodophyta*) and green (*Chlorophyta*) algae. Carotenoids are lipid-soluble compounds consisting of long, aliphatic and conjugated doubled-bonded system usually composed of eight isoprene units (Cha *et al.*, 2008). They can be classified into two types; hydrocarbon carotenoids which are known as carotenes, and oxygenated derivatives named as xanthopylls in which oxygen can be present as OH group (lutein), oxi-groups (cantaxanthin) or in combination of both (astaxanthin, fucoxanthin) (Guedes *et al.*, 2011; Del Campo *et al.*, 2007). Chlorophylls are also lipid-soluble pigments which contain a porphyrin ring. The main types of chlorophylls are chlorophyll a and chlorophyll b, however the sensitivity of these pigments to pH and temperature results in the formation of numerous degradation products such as pheopytins, pyropheophytins, etc. (Pangestuti and Kim 2011b; Hosikian *et al.*, 2010). Due to the lipid-soluble character of both carotenoids and chlorophylls, their extraction has been carried out mainly using organic solvents (acetone, ethanol, hexane) in traditional extraction approaches (Simon and Helliwell, 1998; Domínguez-Bocanegra *et al.*, 2004; Orosa *et al.*, 2005; Van Leeuwe *et al.*, 2006;

Sarada *et al.*, 2006; Cha *et al.*, 2008) or under pressurized liquid extraction conditions (Denery *et al.*, 2004; Jaime *et al.*, 2010). Besides, several works have used a small percentage of water in combination with the main extraction solvent (90 % ethanol/water) to carry out the pressurized liquid extraction of carotenoids and chlorophylls from green algae (*Chlorella vulgaris*) (Cha *et al.*, 2010a; Cha *et al.*, 2010b), or fucoxanthin, which is widely distributed in nature (its contribution to the estimated production of carotenoid in nature is about 10%) and is the principal pigment in brown seaweed (Shang *et al.*, 2011). SWE has been also employed as alternative extraction procedure for obtaining bioactive compounds (carotenoids and chlorophylls between them) from *Haematococcus pluvialis* (Rodríguez-Meizoso *et al.*, 2010) and *chlorella vulgaris* (Plaza *et al.*, 2012). However, no significant amounts of carotenoids and chlorophylls were obtained in the water extract, mainly due to the non-polar nature of these compounds.

Finally, phycobiliproteins, the others pigments found in algae, can be classified in phycocyanins, allophycocyanins and phycoerythrins, being the latter the most abundant in many red algae (Pangestuti and Kim, 2011b). Since phycobiliproteins are water soluble, they can be extracted by SWE; in fact, different works (see section 17.4.1) have demonstrated the presence of these compounds in pressurized water extracts from algae (Herrero *et al.*, 2004, Herrero, *et al.*, 2005; Simó *et al.*, 2005).

#### **17.4.3.5. Therapeutic and pharmacologic products**

Certain species of marine microalgae are able to produce potent toxins, which can be accumulating in filter-feeding shellfish and lead to poisoning fish marine mammals, sea

birds and humans. Some of these toxins, on the other hand, have been suggested as potent anticancer drugs or even as anaesthetic agents.

During the past two decades, a variety of toxins from algae and cyanobacteria have been identified (Dahlmann *et al.*, 2003). According to their chemical structure, toxins may be classified into three main groups: cyclic peptides (microcystins and nodularins), alkaloids (neurotoxins and cylindrospermopsin), and lipopolysaccharides (Msagati *et al.*, 2006).

The chemical structures of toxins are complex and although a high number of them are lipophilic (brevetoxins or okadaic acid), others, for instance domoic acid or saxitoxins, present hydrophilic properties (Pistocchi *et al.*, 2012; Gerssen *et al.*, 2010).

Some reports have shown important pharmacological properties of, for instance, paralytic shellfish toxins such as saxitoxin and neosaxitoxin, which are potent nonprotein neurotoxins which have been studied as potent local (Rodríguez-Navarro *et al.*, 2007) and long term anaesthetic agents (Hille, 1975; Adams *et al.*, 1976); their activity seems related to a selective and reversible blockage of the voltage-gated sodium channels at the neuronal level. For further information on the different structures of neurotoxins, their toxicity and possible biotransformations, readers are referred to a recent publication (Wiese *et al.*, 2010).

On the other hand, other recent studies have suggested the use of microcystins (potent hepatotoxins) as a novel class of anticancer agent. Results from this study showed that microcystin-induced phosphatase inhibition results in potent hepato-cytotoxicity when microcystin compounds can gain intracellular access (Monks *et al.*, 2007).

The solvents employed to extract these toxins include 5 % acetic acid, methanol, acidified methanol, water and mixtures methanol:water (Lawton and Edwards, 2001;

Lawrence and Menard, 2001; McElhiney and Lawton, 2005). Mixtures of methanol:water have been also used as solvent to extract various algal and cyanobacterial toxins (saxitoxin, anatoxin-a, domoic acid, nodularin, microcystins, okadaic acid and dinophysistoxin-1) from phytoplankton (Dahlmann *et al.*, 2003) and aqueous 5 % formic acid was employed to the extraction of cylindrospermopsin for the analysis of blue-green algal food supplements (Liu and Scott 2011). Taking into account that dielectric constant of water at high temperatures is similar to that presented by some organic solvents, such as methanol (Wiboonsirikul and Adachi , 2008), SWE could be potentially be employed as an alternative to solvent extraction of different toxins. In this sense, Aranda-Rodríguez et al. (2005) demonstrated the suitability of PLE and SWE for extracting toxins from *Microcystis aeruginosa* cyanobacterial cells. The results obtained in this work, suggest that water at high pressure and temperature (60-100 °C), can be a good solvent for the extraction of microcystins with a wide range of polarity.

### **17.5 Future trends and conclusions.**

As can be inferred from the data shown above, one of the future trends in the use and applications of SWE (PHWE) is the development of green integrated systems able to perform multi-unit operations such as reaction, extraction, fractionation, etc. Subcritical water extraction can be used in some or all the mentioned operations with some advantages over conventional processes; on the other hand, it can be easily combined with other green solvents such as sub- or supercritical carbon dioxide or ethanol. Related to this, a clear trend is the use of PHWE together with enzymatic catalysis that is, transforming the actual enzyme-assistant-extraction (EAE) to a subcritical water

enzymatic reaction and extraction (SWERE). Although just few examples can be found in the literature by using this approach, it seems clear that by the development of new and thermostable enzymes and new approaches for extracts' fractionation and purification, the development of this technique can be a reality; as already shown in the pioneer work of Turner (Turner *et al.*, 2006; Lindahl *et al.*, 2010), the environmental impact of the developed method using beta-glucosidase and subcritical water extraction is lower in terms of primary energy consumption and global warming potential as compared to a conventional extraction/hydrolysis method based on methanol extraction and hydrochloric acid hydrolysis at 80°C. Considering the wide range of compounds that can be extracted from algae and, at the same time can benefit from the development of integrated processes, it is easy to understand the need of more research in this area; therefore, new ideas and new approaches are expected with the final goal of simplifying, increasing the efficiency and decreasing the risks for the environment and human health. Sustainability will be the target to provide with new answers the challenges we are facing today.

In terms of applications, in this chapter we have tried to provide with an overview of not only the real applications that can be found in the literature in terms of SWE of bioactive compounds from algae (quite scarce nowadays), but also of the different possibilities that the technique offers for the extraction of other valuable compounds (such as peptides, carbohydrates, pigments, compounds with therapeutic properties, etc.) that, even if they have not been approached that way, the use of subcritical water extraction may provide with some advantages over the conventional processes used, at least in terms of efficiency, speed, selectivity, etc.

To conclude, water is the *greenest* solvent in nature and has the potential to replace environmentally burdensome solvents such as acetonitrile, methanol, dichloromethane and toluene at high pressures and temperature. Water can be quite selective by changing the extraction temperature, and processes are quite easy to optimize towards the enrichment of the compound/s of interest; on the other hand, it is important to consider that care must be taken with thermolabile compounds' extraction, although risks can be minimized by a careful optimization of extraction time and temperature. With all these considerations we can conclude that SWE (or PHWE) can be an appropriate choice for many applications requiring a medium to high polarity solvent and for compounds with some degree of polarizability; in those cases, the process can give many advantages that, at the end, can lead to a more efficient, environmentally friendly and sustainable extraction process.

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## Figure Captions

**Figure 1.** Dielectric constant ( $\epsilon$ ) of pure liquid water as a function of the temperature, and values corresponding to some common organic solvents at room temperature.

**Figure 2.** Scheme of the main parts contained in a static SWE.

**Figure 3.** Fucoidans structure from *F. vesiculosus*, composed mainly by a disaccharide motif containing sulfate at the 2-position of the 3-linked fucose and sulfate groups on the 2- and 3-positions of the 4-linked fucose. Adapted with permission from (Jiao *et al.*, 2011). MDPI Open Access.







